

CLEANkER by calcium  
looping for low-CO<sub>2</sub> cement



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Workshop on the Development of Efficient CO<sub>2</sub> Capture Technologies for Cement  
and Lime Industries

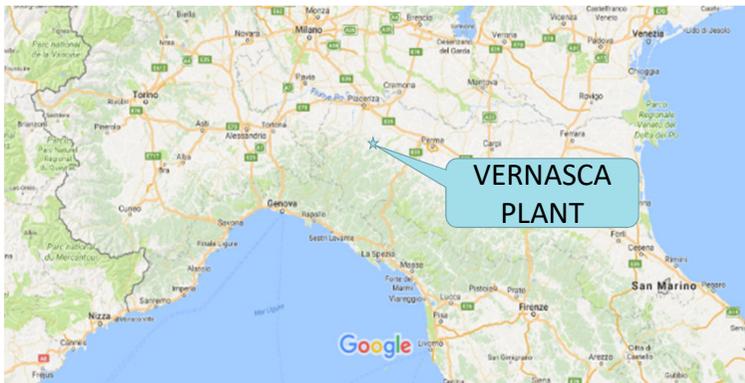
# Integrated Calcium Looping Technology for the Cement Industry and Status of CLEANKER Pilot Plant

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# The CLEANKER project – Primary project objectives

The ultimate objective of CLEANKER is advancing the integrated Calcium-Looping (CaL) process for CO<sub>2</sub> capture in cement plants.



This fundamental objective will be achieved by pursuing the following primary targets:

- Demonstrate the integrated Calcium-Looping process at TRL 7, in a new demo system connected to the operating cement burning line of the Vernasca 1.300.000 ton/y cement plant, operated by Buzzi Unicem in Italy.
- Demonstrate the technical-economic feasibility of the integrated CaL process in retrofitted large scale cement plants through process modelling and scale-up study.
- Demonstrate the storage of the CO<sub>2</sub> captured from the CaL demo system, through mineralization of inorganic material in a pilot reactor of 100 litres to be built in Vernasca, next to the CaL demo system.



# The CLEANKER project – The consortium

**Starting date: October 1<sup>st</sup> 2017**

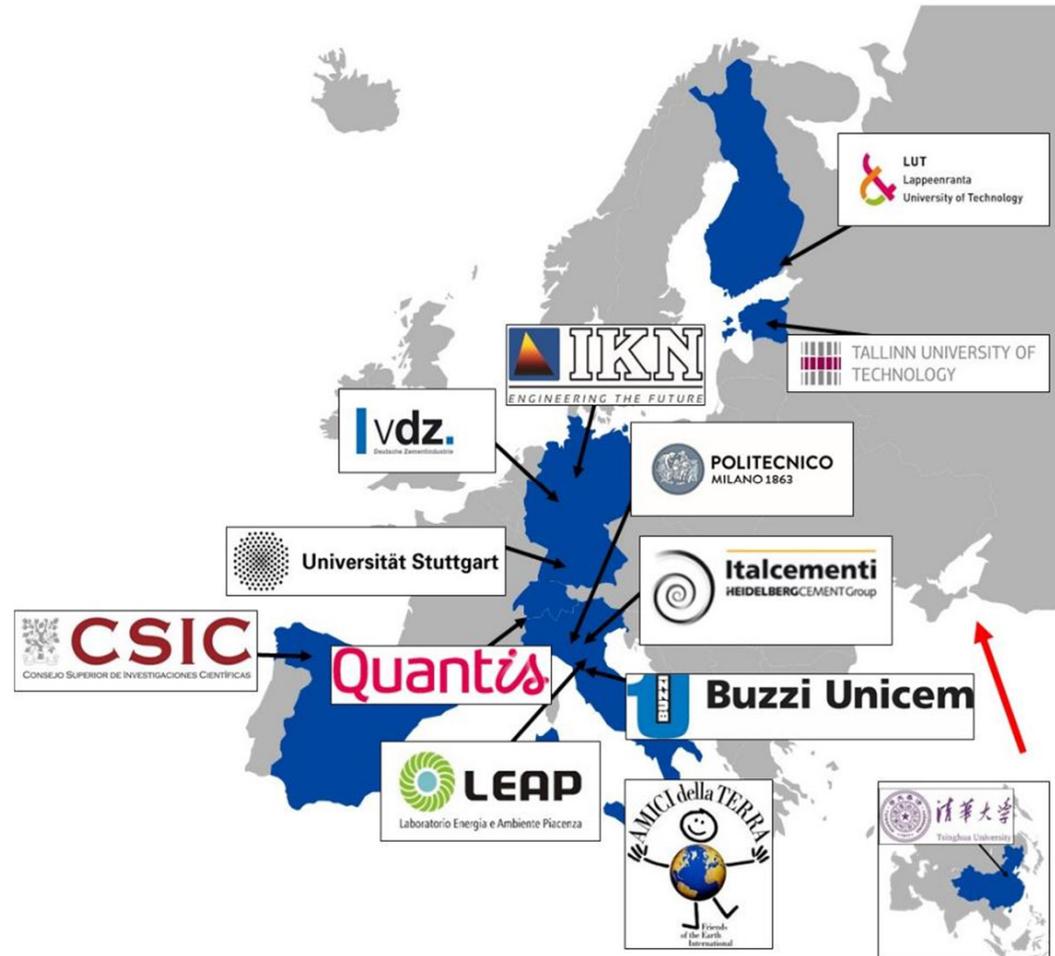
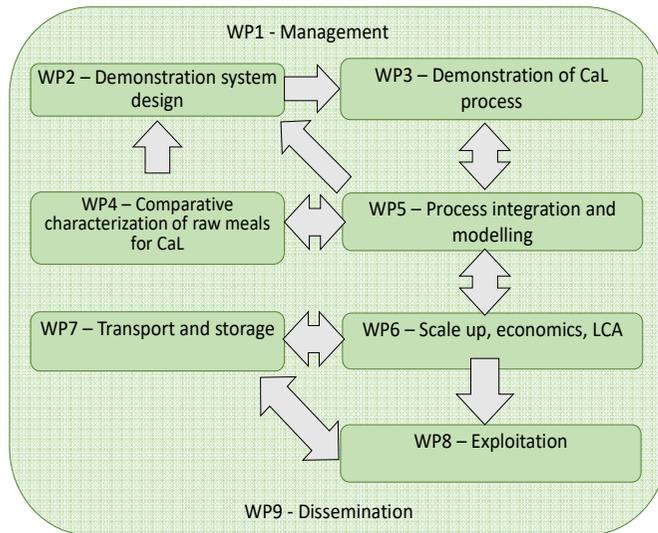
**Duration: 4 years and half**

**Total budget: € 9.237.851,25**

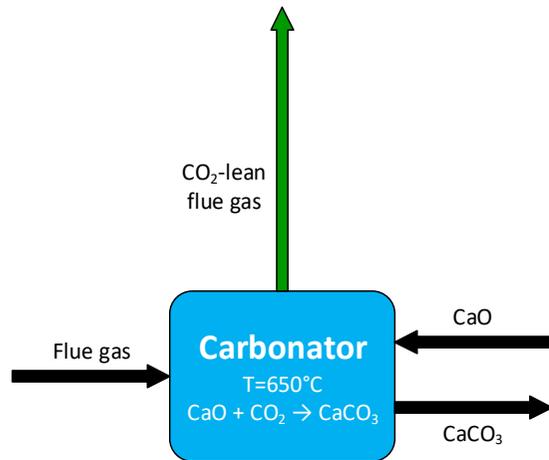
**EU co-financing: € 8.972.201,25**

**Chinese government funding: 265.650 €**

**Partner: 13 from 5 EU member states + Switzerland and China**



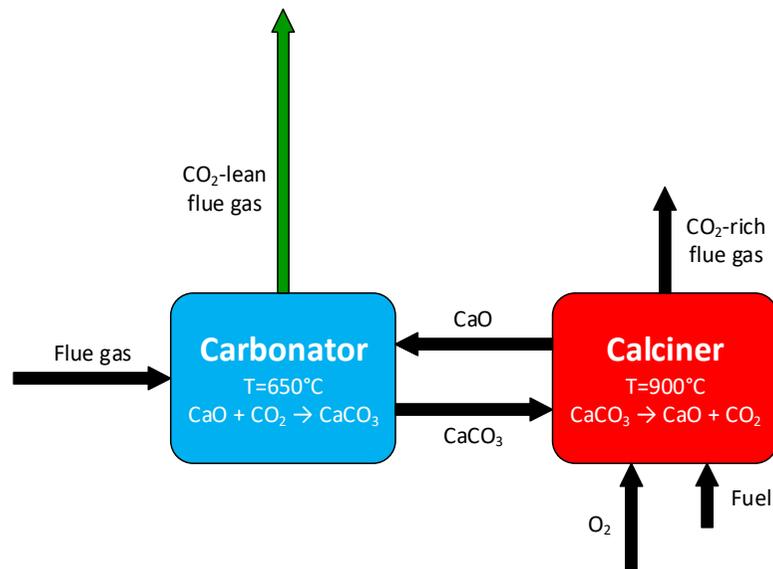
# Calcium Looping concept



- Flue gases enter the carbonator together with CaO, which acts as a CO<sub>2</sub> sorbent
- Carbonation reaction:  
 $\text{CaO} + \text{CO}_2 \rightarrow \text{CaCO}_3 @ 600 - 650 \text{ }^\circ\text{C}$
- CO<sub>2</sub> is selectively captured from the flue gas stream



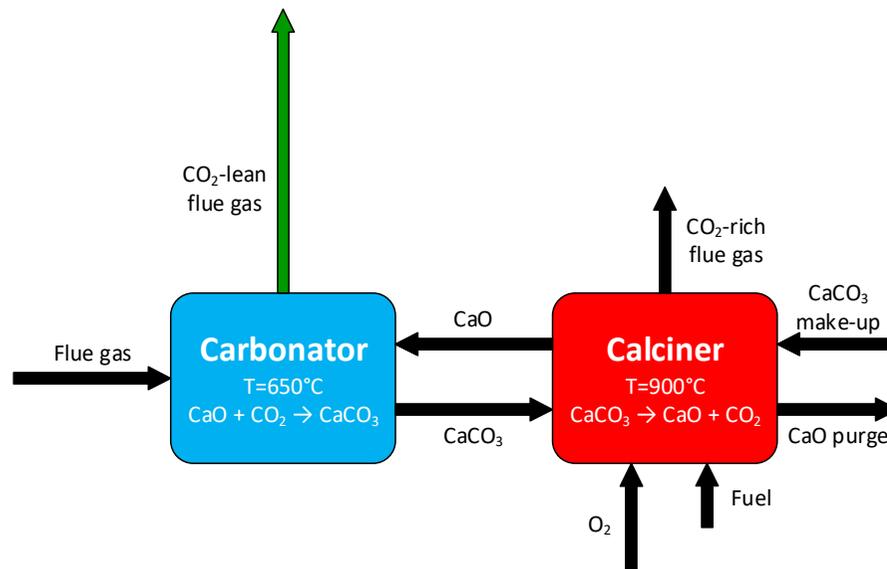
# Calcium Looping concept



- CaO is produced in the calciner, where the opposite reaction is performed and the captured CO<sub>2</sub> is released
- **Calcination reaction:**  
 $\text{CaCO}_3 \rightarrow \text{CaO} + \text{CO}_2$  @ 900°C
- The necessary heat is provided by burning a fuel in pure oxygen  
  
→ Oxy-fuel combustion produces a CO<sub>2</sub>-rich flue gas stream (theoretically, a CO<sub>2</sub> – H<sub>2</sub>O binary mixture)



# Calcium Looping concept

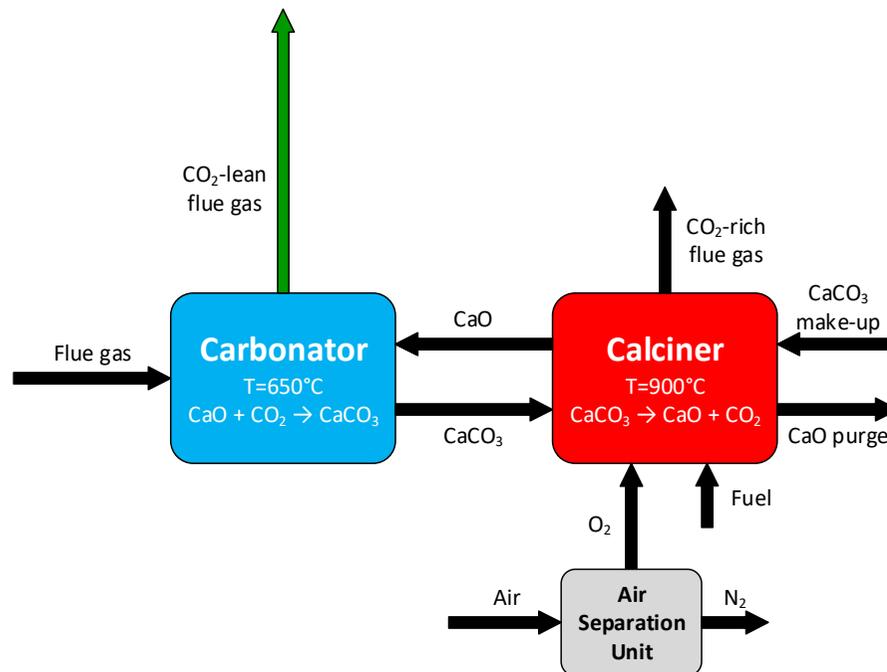


- **Continuous CaCO<sub>3</sub> make-up and CaO purge shall be guaranteed to the calciner, in order to:**
  - Prevent contaminant accumulation
  - Counteract CaO deactivation as a CO<sub>2</sub> sorbent
- **This is the Calcium Looping working principle → for real application some auxiliary units are needed**

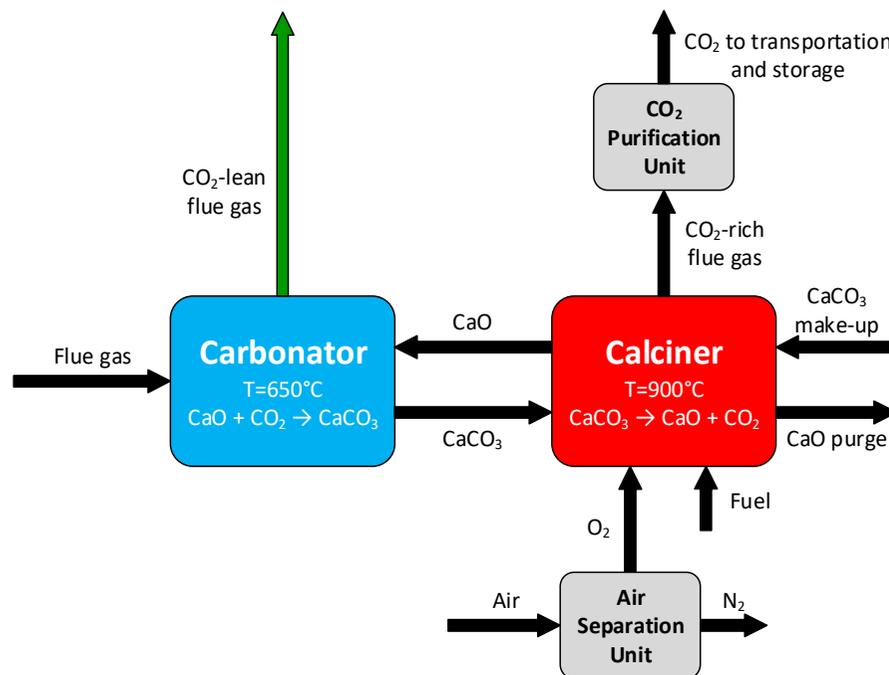


# Calcium Looping concept – Auxiliary plants

- An Air Separation Unit (ASU) is needed to produce the pure oxygen needed by the calciner



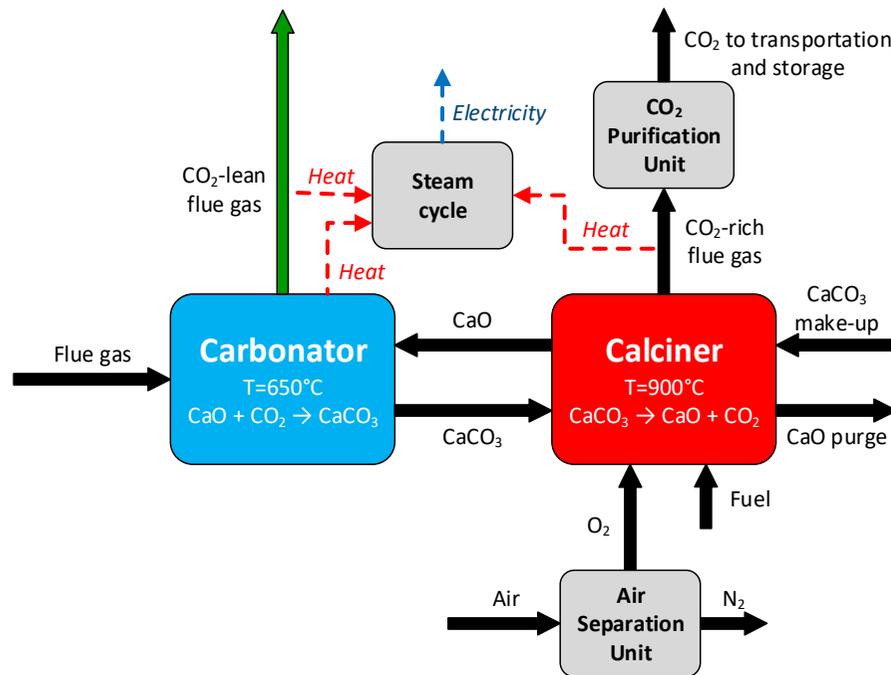
# Calcium Looping concept – Auxiliary plants



- The flue gas stream produced by a real oxyfuel combustion is not a CO<sub>2</sub> – H<sub>2</sub>O binary mixture (because of air leakages, ASU efficiency, actual fuel and sorbent composition...)

→ A CO<sub>2</sub> Purification Unit (CPU) is needed to remove oxygen, other non-condensable species and contaminants unwanted for CO<sub>2</sub> transportation/storage/utilization

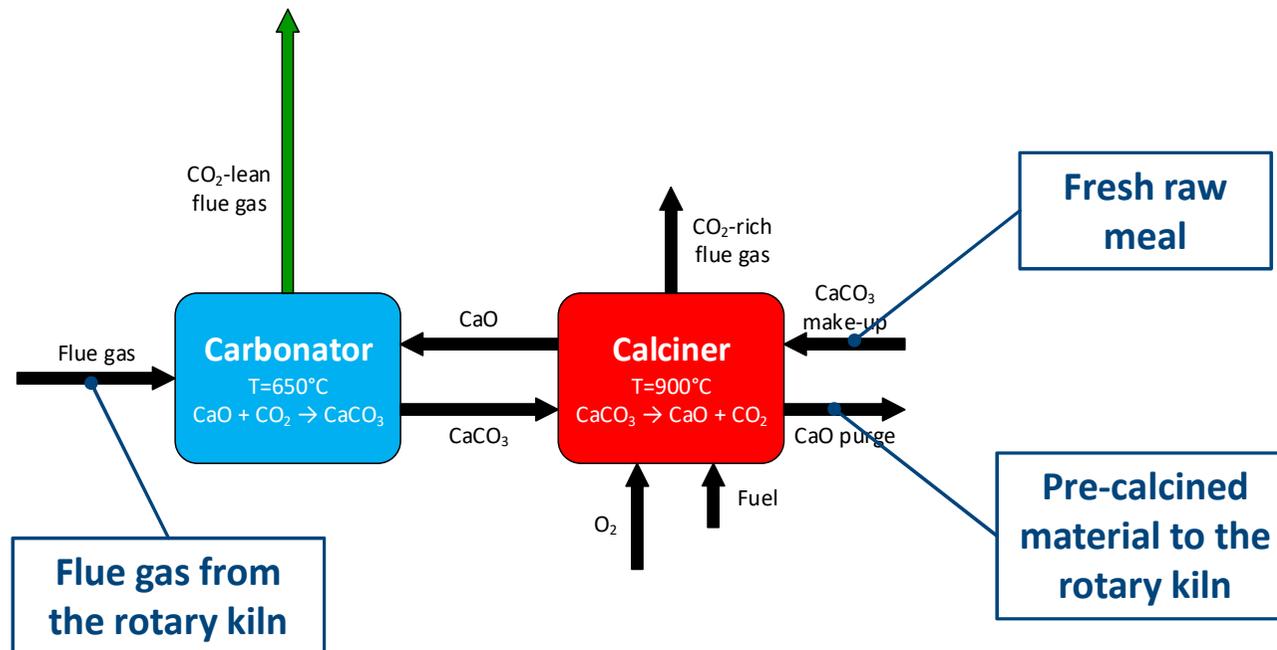
# Calcium Looping concept – Auxiliary plants



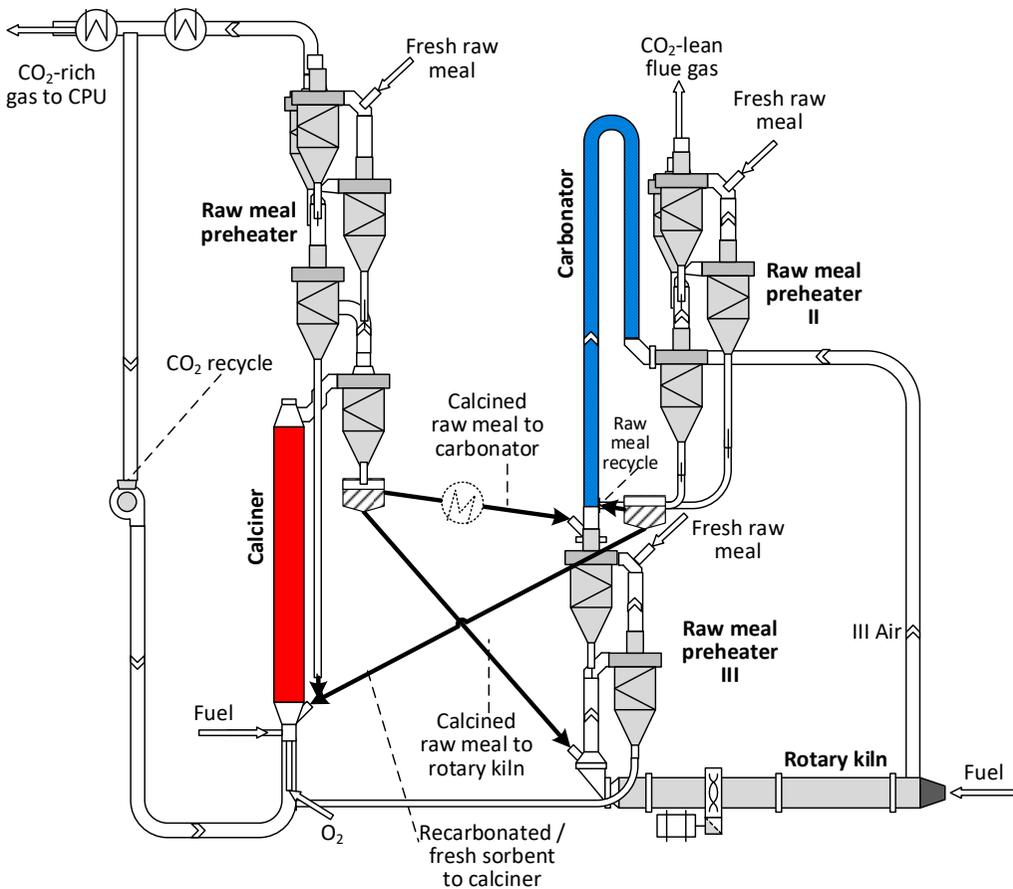
- Given the **high temperatures** involved in the process, **heat can be efficiently recovered in a steam cycle to produce electricity**, thus decreasing the electricity consumption of the capture process

# Calcium Looping in cement industry – Integrated configuration

- The CaL CO<sub>2</sub> capture process can be efficiently integrated in the clinker production



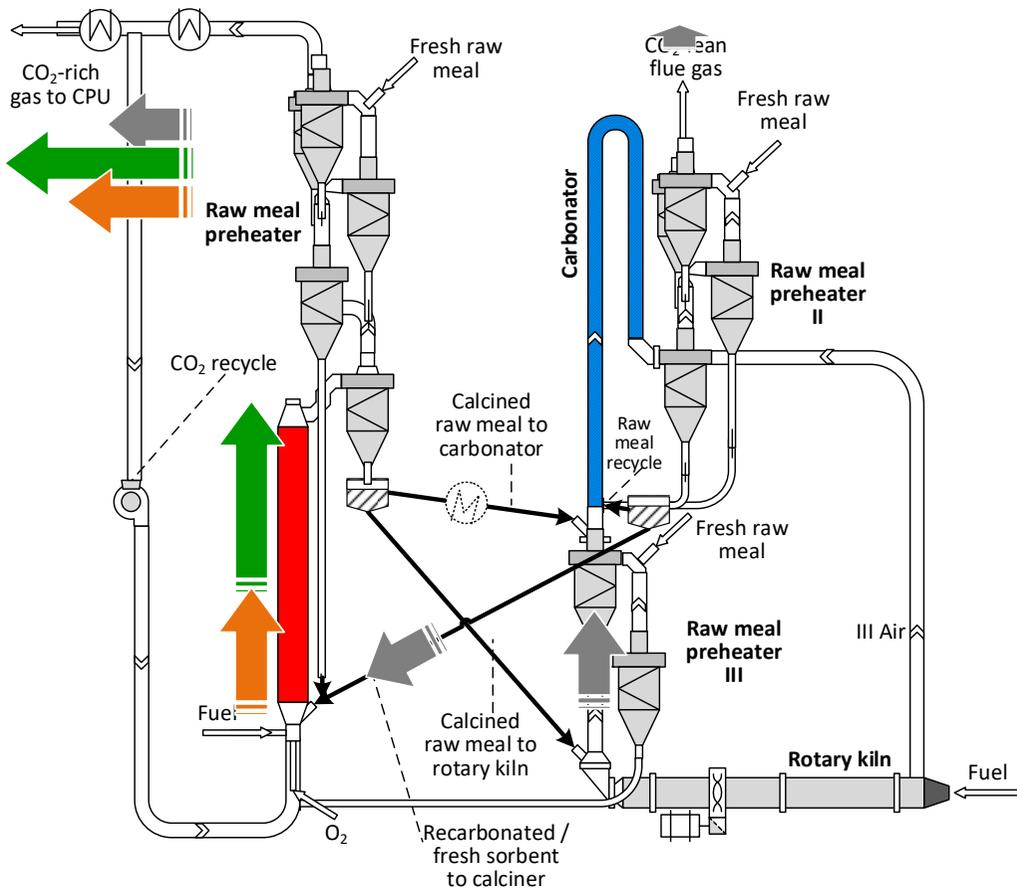
# Calcium Looping in cement industry – Integrated configuration



- **CaL Calciner** coincides with the **cement kiln pre-calciner**, but it operates in **oxyfuel**  
 → **Combustion gas is very rich in CO<sub>2</sub>** (no N<sub>2</sub> dilution)
- **Pre-calcined raw meal is split** to be fed:
  - **To the rotary kiln**, as in conventional plants
  - **To the Carbonator**, where it acts as **CO<sub>2</sub> sorbent** to selectively capture the **CO<sub>2</sub> contained in kiln flue gases**
- The **CaCO<sub>3</sub>** leaving the **Carbonator** is then **recycled to the Calciner**, where the captured CO<sub>2</sub> is released in the CO<sub>2</sub>-rich stream
- The **gas stream** leaving the **Carbonator** is **virtually CO<sub>2</sub>-free**

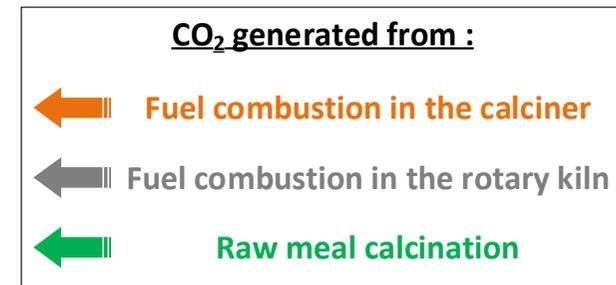


# Calcium Looping in cement industry – Integrated configuration



The integrated Calcium Looping process captures:

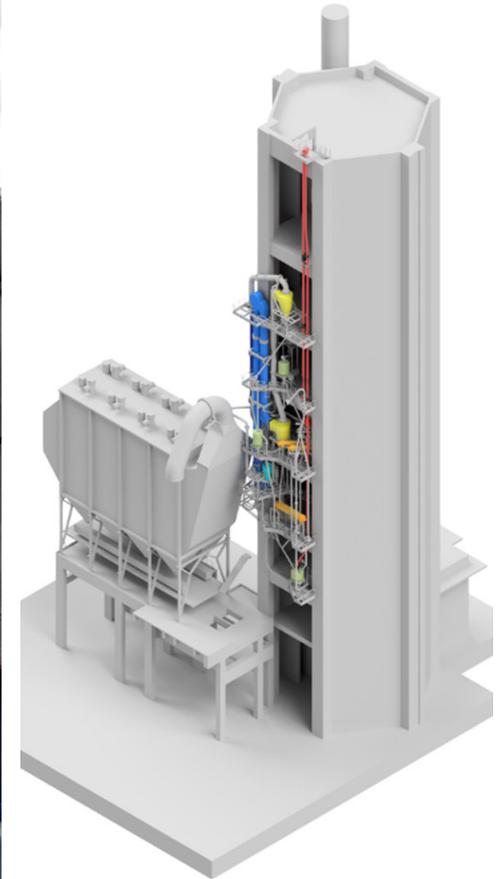
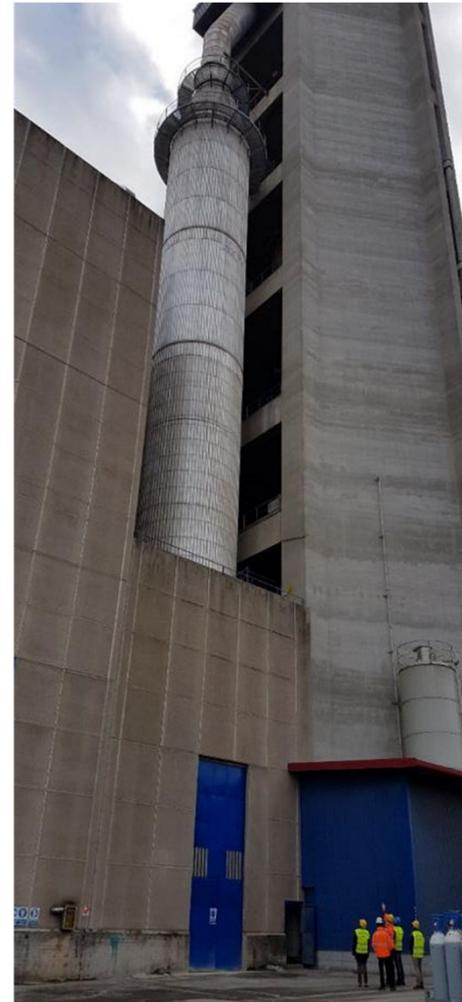
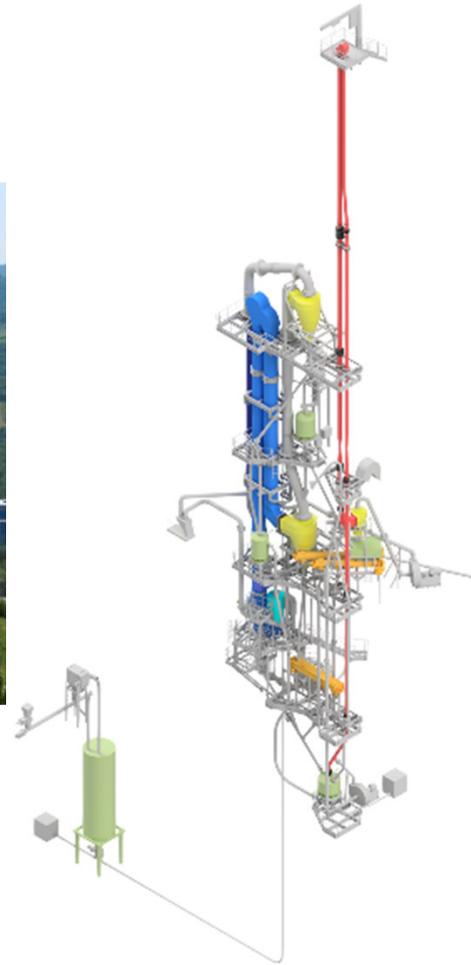
- **All the CO<sub>2</sub> generated in the calciner**
- **The CO<sub>2</sub> captured by the carbonator**  
→ This value depends on **carbonator CO<sub>2</sub> capture efficiency**
- **Carbonator efficiency ~80%**  
→ **global capture efficiency >90%**



# The CLEANKER demo system



Preheater tower



# The CLEANKER demo system



# The CLEANKER demo system – The Carbonator



- Entrained flow reactor in stainless steel
- Gooseneck shape: riser and downcomer, for a total length ~ 105 m
- Diameter: 250 – 350 mm



# The CLEANKER demo system – The oxyfuel Calciner



- Two burners, heavy oil as fuel
- Several oxygen injection points for a better control of temperature profile
- A water-cooled screw heat exchanger cools the material produced by the Calciner to the temperature required by the Carbonator



# Experimental campaigns

- **Nine experimental campaigns have been scheduled:**
    - 5 short tests of three days each
    - 4 long tests of one week each
  - **The aim of the short tests is to identify the most attractive operating conditions for the longer test runs**
- **Particular attention will be given to the analysis of the governing parameters of the CaL process:**
- **Oxidizer for the calcination process: Air/Oxygen**
  - **Calclner outlet temperature**
  - **Type of CO<sub>2</sub> sorbent, i.e. different raw meals**
  - **Gas flow rate at carbonator inlet**
  - **Solid to gas ratio in the carbonator**
  - **Solids temperature at carbonator inlet**



# Acknowledgments

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